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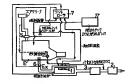
(54) NITROGEN OXIDE REDUCING DEVICE FOR INTERNAL COMBUSTION ENGINE

(57) Abstract:

PURPOSE: To deoxidize and purify the NOx in the exhaust gas directly by the H_2 from a hydrogen generator under the exhaust gas low temperature ambiance so as to reduce the NOx, by composing the system to make a part of a hydrocarbon fuel converted into a hydrogen gas to feed by a reformer catalyst converter.

CONSTITUTION: H₀ is fed near the entrance of a deoxidizer catalyst 2. The air amount is measured by a suction air amount sensor 5 of an engine E to make the H₂ to feed at the same level with the NOx in the exhaust gas. The NOx density in the exhaust gas is found by an NOx sensor 6, and after the NOx flow is calculated from the outputs of both sensors 5 and 6 in a controller 7, the fuel flow led in a reformer catalyst converter, and the reformer catalyst converter temperature by an exhaust gas flow dividing valve 11, and also an air valve 12 for reforming in the system to carry out a partial oxidization, are controlled in order to generate the H₂ corresponding to the NOx flow.

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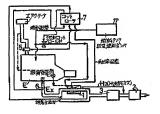
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(54)【桑明の名称】 内燃機関の窒素酸化物低減装置

(52)【學約】

【目的】 リーンバーンエンジンやディーゼルエンジン 等において当該エンジンの燃費の良さを損なうことなく 緋気ガス中の○、の濃度如何を聞わずNO、を有効に還 元浄化し得る内燃機関のNO、低減装置を提供する。 【構成】 内燃機関Eの燃焼室で供給燃料の燃焼による 排気中にNO。とO、の存在のもと、排気系統Ex に設 けH、とNO、を接触反応しNO、を浄化する触媒装置 2の入口側に、メタノール又はLPG、天然ガス等の炭 化水素燃料の一部を改質触媒コンバータによってH。を 生成する水素発生装置1からの日。を供給し、排気系統 の消音装置付近における排気低温雰囲気下で該H。によ り前記継気中のNO、を直接還元浄化して該NO。を効 座良く低減する。



【特許請求の範囲】

【請求項1】 内燃機関の燃焼室で燃料供給装置より供 給された燃料の燃焼による排気中に窒素酸化物と酸素ガ スの存在のもと、鎌気系統内で水素ガスと窒素酸化物を **触媒反応させ、窒素ガスと水に分解するための触媒装置** を設けると共に、該触媒装置の入口側にメタノール又は LPG、天然ガスなどの炭化水素燃料の一部を改質触媒 コンバータによって水素を生成する水素発生装置を設 け、水素ガスを供給可能に構成し、排気系統の消音装置 付近における排気低温雰囲気下で該水素発生装置からの 10 水素ガスにより前記緋気中の窒素酸化物を直接還元浄化 して該審素酶化物を低減するようにしたことを特徴とす る内燃機関の窒素酸化物低源装置。

【発明の詳細な説明】

[0001]

[0002]

【産業上の利用分野】本発明は、内燃機関の窒素酸化物 低凝装置に係り、特に、警藤混合気を使用し、燃料消費 向上をめざす、いわゆるリーンバーンエンジンやディー ゼルエンジン、その他の水素エンジン等において、当該 エンジンの燃管の良さを細なうことなく、绯気中の酸素 20 ガス (以下〇、と称す) の速度如何を問わず窒素酸化物 (以下NO、と称す)を資効に最元浄化しうるリーンN O. 触媒排気浄化システムに関する。

【従来の技術】内燃機関、主としてビストン機関におい て排気の窒素酸化物(以下NO、と称す)の低減方法に は、従来、

- ① 三元触媒によるNOx 低減法
- ② 超希薄空燃比の利用
- ② リーンNOx 無線によるNOx 低減法(例えば、待 30 脚平1-139145号公報〉

の三つが考えられている。しかしながら、**①**の方法はエ ンジンに供給される燃料と空気の重量比が約14.5. 即ち理論空燃比でなければならない。もし理論空燃比よ り燃料が希薄な空燃比を使用するとNO。は低減しな い。しかるに燃料消費の経済性を考えると図2に示すよ うに理論空燃比より希薄側でエンジンを運転した方が燃 料消費率が少なく、効率が良いことが知られている。

【0003】次に②はいわゆるリーンバーンエンジンに よってNO、低減と燃費低減を両立させようとするもの 40 である。しかし、NO、を十分低減できる空燃比を使お うとすれば、燃焼の失火陽界に近づき、エンジンの燃養 が悪くなるばかりでなく、運転が荒れ、ドライバビリテ ょも悪くなる。これを防止するためシリンダ内の空気流 れに乱れや流速増加を計り、燃焼速度を速くして失火限 原をより希薄域になるように改良しようとするものがあ る。しかし、空気乱れや流速増加を過度に行うと、かえ って着火時の火炎核形成や燃焼初期の火炎伝播が妨げち れるため、この方法による失火限界の拡大には限界があ る。また、シリンダ内の空燃化分布を調整して点火栓近 50 。を浄化するための無媒装置を設けると共に、該触媒装

傍のみ着火に適した濃複合気とする方法もあるが、図3 に示すように失火限界がより希薄側に移ると、発生NO 、も砕線で示したように、減少する割合が少なくなるの で大きな効果は期待できない。

【0004】 @は上記@の欠点を締うため、失火限界よ りるる理論事故比に近い教録消費率最低点付近を使って 運転し、やや低減不足のNO。はゼオライト系リーンN O. 触媒で浄化しようとするものである。この方法は燃 費の良いシステムになる可能性がある。しかしながら、 とのリーンNO。触媒は、排気中に大量のO。存在下で NO、を還元することになり、温度条件などが厳しく、 現状では充分な触媒のNO。 浄化率と耐久性が両立しに くいといった実用上解決すべき問題がある。以上のよう にエンジンの燃料消費率を振力小さくできる空燃比を使 いながらNO。を充分低減する方法にはいずれも実用上 の問題が多い。

【0005】ととろでリーンバーンエンジンでもディー ゼルエンジンでも緋気中に遏動の。を含むことは基本的 に同じであるが、このエンジンの緋気は、緋気中にO。 を含み、希薄混合気を使うほどO、焼度は大きくなる。 このようなO。を含む鎌気中のNO。還元浄化を行う触 媒をリーンN○、鮭媒といい、貴金属系、例えばゼオラ イト系の触媒が使われることが多い。このリーンNO、 無媒では、NO。斧化率と温度との関係が図4に示すよ うになっている。そして、350℃以上の高温域は、主 としてHC-NO。の反応である。250~350℃以 下の低温域は、NO、のH、による運元反応となり、N O。の浄化が可能である。

【0006】しかし、リーンNO、触媒は、エンジンの 緋気マニホールド付近に設置されるので、緋気温度が最 高800~900℃にも達し、かつリーンバーンエンジ ンの排気は空燃比が理論空燃比より普藤側を使うので、 継気中に目、は殆ど存在しない。従って、従来. 低温側 の特性は、利用不可能な領域であった。

[00071

【発明が解決しようとする課題】 本発明の目的は、上記 従来の種々の問題を解決するもので、リーンバーンエン ジン又は鴬に〇。(空気)過剰側で運転されるディーゼ ルエンジンの排気中にNO。とO。の共存のもとでリー ンバーンエンジンまたはディーゼルエンジンの燃着の良 さを損なうことなく、緋気中のO。の濃度如何を問わず NO。を有効に還元浄化する排気浄化システムすなわ ち、NO、の放出量を抑制し得る内燃機関のNO。低減 装置を提供しようとするものである。 [0008]

【課題を解決するための手段】本発明の内燃機関のNO ・低減装置は、内燃機関の燃焼変で燃料供給装置より供 給された燃料の燃烧による排気中にNO、とO。の存在 のもと、绯気系統内でH。とNO、を触媒反応させNO 置の入口側にメタノール又はLPG、天然ガス等の炭化 水素燃料の一部を改質触媒コンバータによって水素を発 生する水素発生鉄體を設けてH」を供給可能に構成し、 鎌気系統の消音装置付近における鎌気低温雰囲気下で該 水素発生装置からのH、により前記排気中のNO。を直 接還元學化して該NO、を低減するようにした構成であ る。

3

[0009]

【作用効果】上記構成からなる本発明の内燃機関のNO 、低減終層は 以下の作用を奏する。

【①①10】すなわち、本発明者等が案出した本発明の 内燃機関のNO、低減線置は、図1に示すような構成と することによって、内燃機関の燃焼室で供給燃料の燃焼 による継気中にNO、とO、の存在のもと、H、とNO 。を接触反応させ、窒素ガスと水に分解する鎌気系統に 設けた触媒装置の入口側にメタノール又はLPG、天然 ガスなどの炭化水素燃料の一部を改質触媒コンバータに 導きH、を生成する水素発生装置からのH、を供給し、 様気系統の補音装置付近における緋気低温雰囲気下で該 H、により前記排気中のNO、を効率良く的確に直接還 20 500℃が適当であり、メタノールに混入させる空気流 元浄化して該NO、を低減する作用効果を奏する。この ため、本発明の内燃機関のNO、低減装置は、エンジン の使用空燃比が理論空燃比より過滤側、理論空燃比、理 論空燃此より希藤側と緋気中のO,の存在又はO。の濃 度に関係なくNO、を触媒によって低減できるのでエン* CH, OH + Air - H2

【0018】3) 触媒にCu-MnまたはCu-Znを

用い、メタノールに水蒸気を加えるかまたは空気やメタ ノール水を加え水蒸気改質を行う。温度は2.50°C程度※30

[0020]となる。

【0021】また、LPG、天然ガスなどの炭化水素燃 料を使うエンジンにあっては、触媒としてNI、CO、 Rhを使い、温度300~800℃で改質する。この炭 化水素燃料の場合には、水蒸気や空気や水タンクからの★

> HC + HzO → H, + CH₄ + 00 HC + H, O - H2

CO H a 4. HC + Air -→ H, + CO HC + 排気

* ジン(自動車)性能上、燃費上NO。低減条件を考慮せ ずに最適値を選ぶことができる有利さを持たせ得る。 [0011]

【実施例】実施例における水素発生装置はエンジンに使 用する燃料によって改質触媒コンバータが次のように分

類される。 【0012】すなわち、メタノールを燃料とするエンジ

ンにあっては

1) Pd、Pt. Cu/Cr/N:等の選移金属触媒を 10 用い、メタノールを排気によって加熱蒸発させたガス

を、この触媒に導きH、を生成する。触媒入口ガス温度 は300℃程度が最良であって、この時の反応は [0013]

【0015】2)メタノール蒸気に空気を混合させ、C u-N:-Cr/アルミナ触媒によってメタノールの一 部を部分酸化させ、H』を生成する。温度は400℃~ 置をコントロールし、温度を保つようにする。との場合 の反応は、

[0016] [(£2]

※が適当で、反応は

[0019] [(£3]

★水を加えて改賞を行う。(触媒により温度が異なる。低 温ではメタンが多く、高温ではCOが多い)。反応とし ては

[0022]

[{£4]

+ CO2 300~5000

+ CO2 8000

8000

700% (EGR改質)

[0023]となる。

【0024】また、本実籍例の内燃機関のNO。低減装 置は、前記様気系統の維気管に装備するNO。センサ6 と吸入空気量をンサ5の出力からNO。流量を算出し、 常に満正なり、量を決定し前記水素発生装置としての改 酸化を行う場合の空気量および改質燃料量を制御する機 成とすることもできる。

【0025】さらに、本実総例の内燃機関のNO。低減 禁膏は、当診内燃機器の同転数、吸気管負圧、吸気絞り 弁開度又は燃料供給装置としての頓射ポンプの噴射量等 賃触媒コンバータを加熱するエンジン排気流置又は部分 50 の内燃機関における運転条件を検知できるセンサを具備 し当該センサの出力からNOx 流置を予測演算し前記水 安楽生禁患の改資給雄コンバータに供給する総科量をコ ントロールする学習制御方式にした構成とすることもで # 3.

【0026】しかも、本実施例の内燃機関のNO。低減 禁置は、前記触媒装置の入口側において日、と排気の混 台を均一にするため、ミキサーを具備したり、または、 様気系統の猶音続置を有効利用する構成とすることもで 83.

【0027】詳述すれば、本実施例の内燃機間のNO。 低減続置は、前記従来の問題を解消するために案出され たものでその基本構成図を図しに示す。すなわち、本窓 施例の第1のポイントは、この日、還元が継気低温側で エンジンEの全運転範囲において使用することである。 第2のポイントは、低温側の利用を可能にするため構成 システム中にH、発生器1を組み込むことである。第3 のポイントは、エンジンEの運転状態又は排気中のNO 、量によってH、発生器 1 を制御し、常に継気中NO。 とモルで当畳程度又は過剰のH、が供給できるようにす るととである。

【0028】還元触媒2は高温にさらされるとH。がO 、と反応しH2 - NO2の選択性が失われるので、35 0℃以上にさらされることのないよう消音器3の付近に 配置する。そして、本実絡例は、燃料配管から分岐し、 液量コントロール弁を介して日、発生器としての改質無 娘コンバータに燃料を導入改質してH。を発生させる。 H, は、還元触媒2の入口付近に供給する。供給するH , は、緋気中のNO、とモルで当置程度にするためにエ ンジンEの吸入空気量センサ5によって空気量を測定 し、排気中のNO、濃度をNO、センサ6によってを求 30 め、コントローラ?で両をンサ5、6の出力からNO。 液量を演算した上で、NOx 流量に対応するH2 を発生 させるため改質触媒コンバータに導入する燃料流量や、 排気分流弁による改質無媒コンバータ温度、部分酸化を 行うものでは改算用空気弁の制御を行う構成である。 【0029】図5において、 橋軸は、 NO。 に対するH ,の供給比、縦軸は、NO。の還元率(浄化率)を示 す。NO、に対して等置の(モル)H。を供給すれば、 もしNO、とH、が完全に混合するものとすればNO。 はすべて還元浄化される(理論値)。しかし実際には完 40 全場合されないので還元率は実験値のようになる。理論 より実験値の方が浄化率が良くなっている部分がある が これは鎌気中の水薬気が貴金属系触媒上で分解し日 、に変換していることによる。従って、供給したH、よ り多くの目。がNO、と反応する。 【0030】その他の実験例としては、日、による還元

浄化を行うNO。低減装置において改駕触媒コンバータ の入口側にH。と緋気とを混合ミキシングするミキサー を設置する機能とすることができる。また本実施例のそ は、それぞれ好適な作動温度範囲を持つため、内燃機関 の排気系統において水素発生器を排気マニホールドの出 口に設置した酸化触媒の後段に、また還元触媒は排気が 膨張し温度が200℃以下に下がるマフラー内。 あるい はその下流に設置することができる。 【0031】さらに、その他の実施例としては、水素発

生器のH、を供給してO、共存下のエンジン鎌気中のN O、多番元為化するNO、低減禁煙において、エンジン の排気マニホールド付近に酸化触媒、三元触媒、排気リ アクタ等のHC、COを酸化する手段を持ち、かつリー ンNO、無線としての改質触媒コンバータにPt‐ゼオ ライト系触媒を用いる構成とすることができる。また、 改質触媒コンバータに消音効果を持たせ改質触媒コンバ ータと緋気マフラーを一体化構成とすることができる。 【0032】しかも、H。によるNO。還元を行うNO 、浄化装置において、ディーゼル機関用として改賀触媒 コンバータの上流にスートトラッパ、未燃焼生成物酸化 手段を設置した構成とすることができる。また、本実施 例において、内燃機関はガソリンエンジン、ディーゼル 20 エンジンの他、水素エンジンでも良く、これちのNO。 低減装置に有効に適用し得る。この水素エンジンの場合 は、水素発生装置が必要でなく、燃料としてのH。をコ ントローラを介してバイバス的に供給することにより適 用することができる。 [0033]

【第1実施例】エンジン排気置11のリーンバーンエン ジンに本発明のシステムを適用する第1実施例を図6に 示す。第1 実施例のエンジンE、は、アイドル時の空気 過剰率λ=0.95~1.0(理論空燃比より令令過滤 側が理論空総比)各回転数の全負荷時および急激加速時 はλ=0.8~1.0 (過滤側)、これ以外の運転条件 $は\lambda = 1.2 \sim 1.8$ の希藤側で運転するエンジンE、 である。従って、緋気中の○、は、り~10%程度まで 変化する。緋気系統E、は、緋気マニホールド8の出口 に酸化触媒9を設置し、HC、CO等の不完全燃練生成 物を酸化し浄化する構成である。さらに、精音器として のマフラー13の下流側に還元無線12を配置する。還 元触媒12の入口には日、と鎌気との混合を均一化する ためミキサー10が設けられている。

【0034】H。発生器11は、図7、図8に示すよう に改置触媒 1 4 を用いた水電解目、発生器である。 【0035】水素発生器11は分岐された排気管内にコ イル状のインナーコアを形成し、インナーコアの一端に はメタノールを噴射する電磁燃料噴射弁が設けてあり、 他端はミキサーに導かれている。インナーコアの入口付 近はメタノールを蒸発させるための多孔セラミックが充 鎮してあり、その後にはペレット状の改質触媒が詰まっ ている。(モノリス状の軸媒を使うとまはインナーコア をコイル状から直線状に変更する。) 触線はPdを使っ の他のNO、浄化参麗である水素発生器および触媒装置 50 ている。図6中、15はエンジンE、への空気量を測定 する吸入空気量センサで、16は排気中のNO、線度を 測定するNO、センサである。

【0038】本第1突施側の場合、NO、とモルで当置の日、企必要とするので、エンジンE、の様気中のNO、、遺族にもよるが、50km/hの車速のときの、31/minのH、。最大出方東大馬力時では1.01/min程度の日、を必要とする。この日、は燃料の一部を改賞して供給されるものであるが、それぞれの運転条件でにおける消費日、が走行投資に及ばすま変まは1~2分以下であり、リーンバーンエンジンを使う燃養低深メリ 10 × 15~2 0%に比べれは燃料できる程度であり、リーンバーンエンジンの低速音特性を損なうことがない。

- [0037] また、H, 発生に要するメタノールは、5 0km/h走行で0.151/min(蒸気) 程度である。
- [0038]以上のように本第1実施側は、少量の燃料を日、染生割11において改質して憲元規制12の低温 物特性を利用して、H、一NO、還元を行うので、エン ジント、の運転空気退制率入に無関係にNO、の低減が 計れる実現上省差歳なリーンパーンNO、低減システム 20 である。また、H、と共に副生するCOはシフト反応 [0039]
- [(£5]
- CO + H, O H: F CO₂ [0040]でH, に変換するか、またはP d機により H, とCOとに分離し、高純度なH, として運元触媒! 2の前方に供給する方法もある。しかし、副生するCO
- は微量であり、そのまま還元剤として還元触媒12の中 で働くことができ、COを放出することはない。

[0041]
第2素施利 第2素施利は、空源用、発電用等に使う
ガスエンジンの場合である。燃料は天然ガスの場合を示
す。とのような目的の理避用エンジンは自動量用と異な
り、一定回転数、一定自衛で載をされる。後で、改質
触媒コンバータの温度は一定に保ち易い。第2実総例の
構成は図りに示すように耐起期1 実施例とほぼ同一であ
るので、同一部分は同一帯を付して限制を含むする。
[0042]水素発生器に供給する燃料は第1実施例と
異なり、天然ガスであり、空気と複合して供給する必要
な日、全位大力である。なり、天然ガスとも影響中によ
40でコントロールする。コントロールは、研起第1実施
例とほぼ間に接て、前記第1実施例とはは可能の作用効果を奏ぎる。

[0043]

【第3条施例】朝記各条約所において、燃料の一部を改 質してけ、を発生させる終置とゼオライト系触媒を組合 せ、NO、を選売学化するエンジンのNO、低減終歴 は、H、の供給条件、内容化よってNO、低減性能に大 きな差異を生じることが分かってきた。図10に示すよ うに、NO、O、全含セエンジンの財気を機能(後 し、改質無償コンバータの上能から日、を供給した場合 のNO、冷化率を図11に示す。図11において債職は NO、に対する日、の供給給給を示し、1.0は、NO 、とH、が当量の場合である。総輸は適元によってNO 、が伸化される割合であって、1.0はNO、かすべて 冷化されてようことを示す。

【0044】図10に示す改質無線コンパータ60内に、図12に示すペレットタイプの触線も1が入っている場合は図14から分かるように高い浄化率を示す。図13に示したモノリスタイプの触媒を2にすると、同じ捐、供給量であっても浄化率は低下する。

【0045】図12に示したペレットタイプの触線61 は、入口で日、と繋気ガスとが十分現合せず、日、に濃度分布があっても迷路のようなペレットの隙間をガスが 値道して行く過程で十分混合し、日、と鉄気ガスが均一 化される。

と、ベルットタイプは振動化とってベレットが互いに飲 れ合って物末化し易いこと、ガスの喧谐断面積が小さ 30 く 温差低がか大きく、排圧増大を招き、エンジン性能 自身を悪化する欠点がある。従って、触媒にはモノリス タイプを使うことが望ましいが、この場合にはH。の供 総化工手が必要化なる。

【0047】一方、エンジン鎌気システムとして見る

[0049] 噴出ノズル63の挿入管外径 dと排気管6 5の内径Dとは dがDの20 が以上必要で、 dを大きく すると複雑の総積が大きくなるので図16 に示すように 鉄気管65の一部を新面拡大形成する、又、噴出ノズル 63から砂質触線コンバータ60までの距離しば Dの少 なくとも2 倍以上を必要とし、10 倍以上大きくしても 50 改善効果は少ない。複合無関は、上述の他に、構成を図 50 な

17. 図18に示すようにすることができる。すなわ ち、H、を繊維させる部分は、小径のH、噴出ノズル6 6とこれより大径で壁部に複数の噴出孔67を設けた有 底筒68とから成るほぼ2重管状に構成されている。噴 出した日、は、まず、日、噴出ノズル66に緋圧の動圧 によって流入する排気と混合し、有底筒68の内筒かち 外衛に輸出し、内外衛の間を流れる排気により更に混合 する。このように2段階の混合過程を経るのでほぼ目。 と排気が完全に均一混合することができる。

【0050】内外筒の大きさ(直径、または断面積)は 10 混合に大きく影響し、内筒が小さいとほとんどの排気は 外筒を塗れ、十分動圧を利用できない。図17. 図18 に於いて内外筒の直径比はD/a (外筒/内筒)は3~ 7程度が有効で2付近が最良である。

【0051】上記構成からなる第3実総例は、混合が良 好となり、モノリスタイプであってもペレットタイプ同 機の浄化率を得ることができる。同一浄化率において供 給H、置を30~60%節約することができるので、H 、発生に要する燃料を少なくでき、エンジンの出力や燃 費への影響を軽減できる。

【0052】倒えば、1、61のリーンバーンガソリン エンジンにおいて通常の運転域代表点で評価すると、エ ンジン回転数2000 грм、トルク40 Nm. この時 のNOx 放出量(). 4.4.1/m + n. このNOx をH. 表示で浄化するのに要するH、複質は、0.661/m 1 n. (). 661/m + n のH, を発生させるのにH, 発生器への燃料は0.331/m+nの燃料蒸気になる (メタノールの場合)。

【0053】D/a=2である図17、図18に示す袋 等量の0.441/m:n程度で済み、燃料は0.22 1/m:nの蒸気0.221/m:nの蒸気に低下す。 る。即ち0.111/minの節約となる。 [0054]

【第4実施例】前記実施例においてゼオライト系触媒を 用い、水素発生器によって水素を発生させ、Have をゼオ ライト系触媒の入口に供給しH」によるNO。 還元を行 えば排気中に高濃度のO、が存在していても大きなNO 、浄化率が得られる。

【0055】しかし、従来のNO、触媒、例えば三元無 40 媒、Cu-ゼオライト系触媒に比べると低温の反応であ って、従来の触媒がSV値(通過ガス流量1/hrと触 媒体積!の此)50,000~100,000を使って いるのに比べると反応速度の関係からより小さなSV (例えば10、000~60、000) を使わなくては ならない。このシステムを車載する場合、本システムの 改質触媒コンバータは入口ガス温度から排気系統の下 強、例えば様気マフラー付近になる。しかるに車輌に於 いては車輌構造上SV値の大きい(コンバータの大きさ の大きい) 改賀触媒コンバータを設置する場所になって SO ジンの鎌気にH,を混合してNO、低減のリーンNO、

おり、すべての車輛へは適用し難い。

【0056】本第4実施例は、改質触媒コンバータの設 置を容易にするため、リーンNO、触媒をマフラーに内 蔵させコンパクト化を計るためのマフラー構造およびマ フラーに触媒を内蔵させても温度条件からNO、浄化を 可能とするものである。

【0057】すなわち、第4実施例の構成は、図20、 図21に示すように、緋気マフラー80にリーンNO。

触媒82を内蔵させるとNO。コンバータと、排気マフ ラーを直列に配置することなく片方で済むため、配置ス ペース的に極めて有利となる。図20、図21に排気マ フラー80にモノリス鮟媒82 (Pt-ゼオライト系) を内蔵した消音効果を持たせた改質触媒コンバータ83 を示す。

【0058】改響触媒コンバータ83の上流よりH、を

複入混合された排気が矢印方向より流入し、ミキシング プレート84に衝突し、このミキシングプレート84の 大小複数の流通孔85を通過して绯気と日。が十分混合 しながちモノリス触媒82に流入する。ミキシングプレ 20 ート84には排気流速最大になる中心部に流通孔85が 設けられていないので、H。がモノリス中心部に集中す ることはない。ミキシングプレート84の流通孔85 は 大小それぞれ直径を翼にして海紗配列されているの で通過激速が異なり、ガスの規律が起こると共に干渉に

【0059】ととろで、排気マフラーはエンジン排気系 練の最後屋に配置されるのが一般的で、 様気マフラーの 入口ガス温度は途中で冷却されるので低くなる。入口温 度が最も高いエンジンの最高回転数最大馬力時でも15 置によって複合促進を行えば、14、の供給置はNO。と 30 0~200℃であり、通常使用頻度の高い運転条件では 100~150℃程度である。

よって消音効果を表する。

【0060】従来の三元触媒やCu-ゼオライト系のリ ーンNO、触媒では300~400°C以上でないと十分 な反応が期待できないからマフラー内に触媒を内蔵させ ることはできない。前記実施例において、月、による運 元を行えば低温で浄化できることを示したが、温度は1 50~300℃程度であって排気マフラーの入口温度と 比べればやや高い温度範囲にある。

【0061】本発明者等は、O、共存下でH、を供給す るNO、低減触媒の活性について能媒成分として何を選 定するべきかを種々実験的に検討した。その結果、P d. Rhは活性が全くなく、Cuは活性が悪く、Ptが 高い活性を示すことを見出した。ただし、Ptは高分散 である必要があり、そのためには高比表面積 (少なくと 6100m* / g以上)を有するアルミナ、シリカ、ゼ オライト等の組体が必要である。

【0062】更に、本発明書等は、NO。低減のリーン NO、触媒およびH、混合以前に行うべき前処理につい て種々に検討を行った。その結果を図19に示す。エン

を示す線図

11 触媒(Pt系)に導くと図19中、曲線Bに示すように 活性の最高点は250℃付近にある。

【0063】アフターバーナ、リアクス、三元触媒、酸 化触媒等をエンジンマニホールド付近に酸け、COH Cを酸化し予め低媒幹を上び続に引、を概念しが3、低 減の改質無線コンバータに導くと図19中曲線Aに示す ように活性速度が低温側にファトし、100~150℃ で臨い活性を示すとをを解かに見出した。

10064)との温度は、排気マフラーの入口温度と一致し、排気マフラー80内にドセーゼオライト系の還元 10 無線80を内蔵することにより初めて可能ならしめた。 既に、HC、COを辞去した後にリーンNO、触媒によるNO、浄化を行った方が浄化率も改善でき、HC-O 、の不完全を反応から無線上にススを形成することもな

[0065] 更にモノリス触媒 82の後に干渉チューブ Ex1を設置することにより消害効果をより良好にして いる。図22は図20、図21と同様の作用効果を奏す るもので、ミキサー部の形態を前記ミキシングブレート と異にし、中空間状部材であるミキシングバイブ86と 20 した点が異なる。上記様成からなる第4字帳例は、改質 影媒コンバータ83と辨気マフラー80か一体化構成と することができるので、コンパクトとなり重製性が良好

となる実用的効果を奏すると共に、全運転範囲で高いN

Ox 浄化率を維持できる優れた効果を奏する。 【図画の簡単な説明】

い実用上侵れた作用効果を奏する。

【図1】本発明の実施例の基本構成を示す構成図 【図2】空燃比と燃料経済性の関係を示す線図

【図3】リーンバーンエンジンの熱費とNOxの関係を

示す練図

【図4】リーンNO、鮭媒の特性を示す線図

【図5】 H、供給率とNO、浄化率の関係を示す線図

【図6】本発明の第1実施例接近の概要を示す構成図 【図2】第2書を解除標準におけまり、発生器の接着図

【図7】第1実施例装置における日。発生器の断面図 【図8】第1実統例装置におけるその他の日、発生器の

【図8】第1実銘例装置におけるその他の日、発生器の 要部を拡大して示す構成図 *【図9】本発明の第2実施例装置の概要を示す構成図

【図10】本発明の第3実総例装置の概要を示す構成図 【図11】第3実施例装置に関してNO、浄化率の関係

【図12】第3実施例装置に関してペレットタイプの無 越接成を示す概要図

《福格成を示り 前安凶 【図13】第3実施例装置に関してモノリスタイプの無

媒構成を示す概要図

【図14】本発明の第3実絡例装置の概要を示す縦断面

【図15】本発明の第3実給例装置の概要を示す横断面図

△ 【図16】本発明の第3実施例装置の概要を示す概要図

【図17】本発明の第3実統例装置のその他の例を示す 縦断面図

【図18】本発明の第3実施例装置のその他の例を示す 満断面図

【図19】本発明の第4実統例に関してNOx 浄化率状況を示す線図

【図20】本発明の第4実総例装置の概要を示す縦断面図 【図21】本発明の第4実総例装置の概要を示す横断面

図 【図22】本発明の第4実絡例装置のその他の構成を示す緩断面図

【符号の説明】

E. E. エンジン 1.11 H. 発生器 3.13、80 消音器 30 12.60 運元触媒 9 酸化触媒

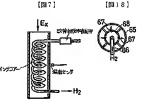
5 吸入空気置センサ 6 NOx センサ

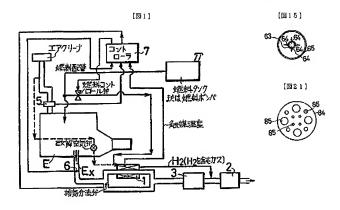
7 コントロール電源 10 ミキサー

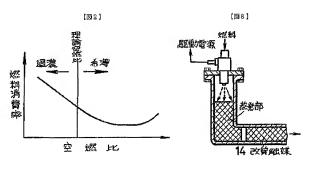
るその間の日、発生器の IV ミキザー

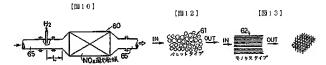
250-350℃ NOx 多 化 率 化 率 化 率

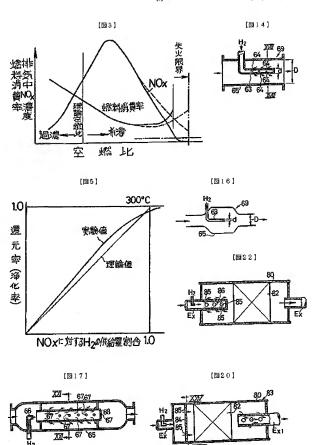
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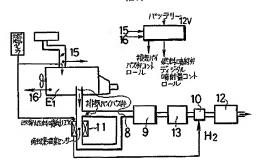




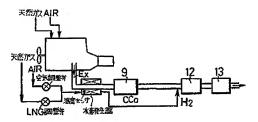


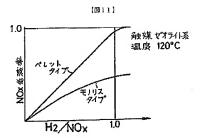


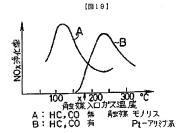
[图6]



[回9]







フロントページの続き

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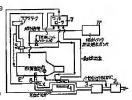
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(54) NITROGEN OXIDE REDUCING DEVICE FOR INTERNAL COMBUSTION ENGINE

(57)Abstract:

PURPOSE: To deoxidize and purify the NOx in the exhaust gas directly by the H2 from a hydrogen generator under the exhaust gas low temperature ambiance so as to reduce the NOx, by composing the system to make a part of a hydrocarbon fuel converted into a hydrogen gas to feed by a reformer catalyst converter. CONSTITUTION: H2 is fed near the entrance of a deoxidizer catalyst

2. The air amount is measured by a suction air amount sensor 5 of an engine E to make the H2 to feed at the same level with the NOx in the exhaust gas. The NOx density in the exhaust gas is found by an NOx sensor 6, and after the NOx flow is calculated from the outputs of both sensors 5 and 6 in a controller 7, the fuel flow led in a reformer catalyst converter, and the reformer catalyst converter temperature by an exhaust gas flow dividing valve 11, and also an air valve 12 for reforming in the system to carry out a partial oxidization, are controlled in order to generate the H2 corresponding to the NOx flow.



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CLAIMS

* NOTICES *

[Claim(s)]

[Claim 1]Both that it is characterized by comprising the following to an entrance side of this catalyst device Methanol or LPG, A hydrogen generator which generates hydrogen by a reforming catalyst converter for some hydrocarbon fuel, such as natural gas, is provided, A nitrogen-oxides reduction device of an internal-combustion engine constituting hydrogen gas so that supply is possible, carrying out direct reduction purification of the nitrogen oxides under said exhaust air with hydrogen gas from this hydrogen generator under an exhaust air low temperature atmosphere in near the silencer of an exhaust system, and reducing these nitrogen oxides.

A basis of existence of nitrogen oxides and oxygen gas during exhaust air by combustion of fuel supplied from a fuel supply system in a combustion chamber of an internal-combustion engine.

A catalyst device for carrying out catalytic reaction of hydrogen gas and the nitrogen oxides inside, and decomposing into nitrogen gas and water.

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DETAILED DESCRIPTION

* NOTICES *

[Detailed Description of the Invention]

[0001]

[Industrial Application]In what is called the lean burn engine and the diesel power plant, other hydrogen fueled engines, etc. which this invention requires for the nitrogen-oxides reduction device of an internalcombustion engine, and use a lean mixture and aim at the improvement in fuel consumption especially,

without it spoils the goodness of the fuel consumption of the engine concerned -- the concentration of the oxygen gas (O₂ is called below) under exhaust air -- it is related with the Lean NO_x catalyst exhaust gas cleaning system which can carry out reduction purifying of the nitrogen oxides (NO_x is called below)

effectively regardless of how. [0002]

[Description of the Prior Art]In a piston engine, as an internal-combustion engine and the Lord, to the reducing method of the nitrogen oxides (NO_v is called below) of exhaust air. The NO_v decreasing method by the use ** Lean NO_x catalyst of the NO_x decreasing method ** super-rarefaction air-fuel ratio by the

former and ** three way component catalyst (for example, JP,1-139145,A) Three ** are considered. However, the weight ratio of the fuel in which the method of ** is supplied to an engine, and air must be about 14.5, i.e., theoretical air fuel ratio. If fuel uses a thin air-fuel ratio from theoretical air fuel ratio, NO_{χ} does not decrease. However, it is known that considering the economical thin side from theoretical air fuel ratio as shown in drawing 2, and it is efficient.

[0003]Next, ** tends to reconcile $NO_{\mathbf{v}}$ reduction and fuel consumption reduction with what is called a lean burn engine. However, if it tries to use the air-fuel ratio which can reduce NO_x enough, it approaches the misfire limit of combustion, and engine fuel consumption not only worsens, but it will be ruined and drivability will worsen. In order to prevent this, disorder and the increase in the rate of flow are measured with the air flow in a cylinder, the rate of combustion is made quick and there are some which are going to improve a

efficiency of fuel consumption specific fuel consumption has few directions which operated the engine by the

misfire limit so that it may become a thin region more. However, since the flame kernel formation at the time

of ignition and the flame propagation in early stages of combustion will be barred on the contrary if air disorder and the increase in the rate of flow are performed too much, there is a limit in expansion of the misfire limit by this method. Although there is also the method of making it into the rich mixture which

adjusted the air-fuel ratio distribution in a cylinder and to which only the neighborhood of an ignition plug was suitable for ignition, since the decreasing rate will decrease as the dashed line also showed generating NO_v if a misfire limit spreads to a thin side more as shown in drawing 3, a big effect is not expectable. [0004]** In order to compensate the fault of the above-mentioned **, it is going to operate using near [slightly near theoretical air fuel ratio] a specific-fuel-consumption minimum score from a misfire limit, and NO_v in which reduction is a little insufficient tends to purify with a zeolite system Lean NO_x catalyst. This method may become a fuel-efficient system. However, there is a problem which should be solved practically that NO_v purifying rate and endurance of catalyst this Lean NO_v catalyst will return NO_v under a lot of O₂ existence during exhaust air, severe [a catalyst] temperature conditions etc. and sufficient under the present circumstances can be easily incompatible. The method of reducing NO_{χ} enough all has many practical problems, using the air-fuel ratio which can make engine specific fuel consumption small as much as possible as mentioned above. [0005]By the way, although it is fundamentally the same that excess O2 is included during exhaust air also by the lean burn engine or a diesel power plant, O2 concentration becomes large, so that exhaust air of this engine uses a lean mixture including ${\sf O_2}$ during exhaust air. The catalyst which performs ${\sf NO_x}$ reduction purifying under exhaust air containing such O, is called Lean NO, catalyst, and the catalyst of a preciousmetals system, for example, a zeolite system, is used in many cases. In this Lean NO, catalyst, the relation between NO_x purifying rate and temperature shows drawing 4. And a not less than 350 ** pyrosphere is

 ${
m NO}_{
m X}$ catalyst is installed near an engine exhaust manifold, and an air-fuel ratio uses a thin side from theoretical air fuel ratio in exhaust air of a lean burn engine, ${
m H}_2$ hardly exists during exhaust air. Therefore, the characteristic by the side of low temperature was a field which cannot be used conventionally. [0007] [Problem(s) to be Solved by the Invention]The purpose of this invention is what solves the above-mentioned conventional various problems, Without spoiling the goodness of the fuel consumption of a lean burn engine or a diesel power plant under coexistence of ${
m NO}_{
m X}$ and ${
m O}_2$ during exhaust air of a lean burn engine or the diesel power plant always operated by the ${
m Oover}_2$ (air) side, the concentration of ${
m O}_2$ under exhaust air — it is going to provide ${
m NO}_{
m Y}$ reduction device of the exhaust gas cleaning system, i.e., the internal-combustion

mainly a reaction of HC-NO_x. A low temperature region 250-350 ** or less serves as a reduction reaction by

[0006]However, since an exhaust-gas temperature amounts also to a maximum of 800-900 ** since a Lean

H₂ of NO_V, and purification of NO_V is possible for it.

[8000]

regardless of how.

[Means for Solving the Problem] NO_{X} reduction device of an internal-combustion engine of this invention, A basis of existence of NO_{X} and O_{2} during exhaust air by combustion of fuel supplied from a fuel supply

engine which can control the burst size of NO_x , which carries out reduction purifying of the NO_x effectively

system in a combustion chamber of an internal-combustion engine, Form a catalyst device for carrying out catalytic reaction of $\rm H_2$ and the $\rm NO_{\chi}$ within an exhaust system, and purifying $\rm NO_{\chi}$, and. Provide a hydrogen generator which generates hydrogen by a reforming catalyst converter for some hydrocarbon fuel, such as methanol or LPG, and natural gas, in an entrance side of this catalyst device, and $\rm H_2$ is constituted so that supply is possible, It is the composition of carrying out direct reduction purification of the $\rm NO_{\chi}$ under said exhaust air by $\rm H_2$ from this hydrogen generator under an exhaust air low temperature atmosphere in near the silencer of an exhaust system, and having reduced this $\rm NO_{\chi}$.

[0009]

[Function and Effect] NO_X reduction device of the internal-combustion engine of this invention which consists of the above-mentioned composition does the following operations so.

[0010]Namely, NO_X reduction device of the internal-combustion engine of this invention which this invention person etc. invented, The basis of the existence of NO_X and O_2 during exhaust air according to combustion of supply fuel in the combustion chamber of an internal-combustion engine by having composition as shown in drawing 1, Carry out the catalytic reaction of H_2 and the NO_X , and to the entrance side of nitrogen gas and the catalyst device formed in the exhaust system decomposed into water Methanol or LPG, H_2 from the hydrogen generator which leads some hydrocarbon fuel, such as natural gas, to a reforming catalyst converter, and generates H_2 is supplied, The operation effect which carries out direct reduction purification of the NO_X under said exhaust air exactly efficiently by this H_2 under the exhaust air low temperature atmosphere in near the silencer of an exhaust system, and reduces this NO_X is done so. For this reason, NO_X reduction device of the internal-combustion engine of this invention, Since an engine operating air-fuel ratio can reduce NO_X according to a catalyst regardless of the concentration of existence of O_2 a thin side and under exhaust air, or O_2 from a rich side, theoretical air fuel ratio, and theoretical air fuel ratio, from theoretical air fuel ratio On engine (car) performance, The profitableness which can choose an optimum value without taking into consideration fuel consumption top NO_X reduction conditions can be given.

[0011]

Example]A reforming catalyst converter is classified according to the fuel which uses the hydrogen generator in an example for an engine as follows.

[0012]That is, if it is in the engine which uses methanol as fuel, the gas which carried out heating evaporation of the methanol by exhaust air is led to this catalyst using transition metal catalysts, such as 1Pd, Pt, and Cu/Cr/nickel, and H₂ is generated. About 300 ** is best and catalyst inlet gas temperature is a

reaction at this time. [0013]

[Formula 1] $C H_3 O H \rightarrow C O + 2 H_2$

[0014]It becomes.

[0015]2) Make methanol vapour mix air, according to Cu-nickel-Cr/alumina catalyst, carry out partial

oxidation of some methanol, and generate H_2 . 400 ** - 500 ** are suitable for temperature, it controls the air flow rate made to mix in methanol, and maintains temperature. The reaction in this case, [0016] [Formula 2]

$$CH_3OH + Air \rightarrow H_2 + CO + H_2O$$

[0017]It becomes.

[0018]3) Cu-Mn or Cu-Zn is used for a catalyst, and add a steam to methanol, or add air and methanol water, and perform steam reforming. About 250 ** is suitable and temperature is a reaction. [0019] [Formula 3]

$$C H_3 O H + H_2 O \rightarrow 3 H_2 + C O_2$$

[0020]It becomes.

[0021]If it is in the engine using hydrocarbon fuel, such as LPG and natural gas, nickel, CO, and Rh are used as a catalyst and it reforms at the temperature of 300-800 **. In the case of this hydrocarbon fuel, the water from a steam, air, or a water tank is added, and refining is carried out to it. (Temperature changes with catalysts.) There is much methane at low temperature and there is much CO at an elevated temperature. As a reaction, [0022]

```
[Formula 4]
```

[0023]It becomes.

 $[0024]NO_\chi$ reduction device of the internal-combustion engine of this example, NO_χ flow is computed from the output of the NO_χ sensor 6 with which the exhaust pipe of said exhaust system is equipped, and the suction-air-quantity sensor 5, It can also have composition which controls the air content and the amount of reforming fuel in the case of performing the engine exhaust gas flow or partial oxidation which determines the always proper amount of H_2 and heats the reforming catalyst converter as said hydrogen generator. $[0025]NO_\chi$ reduction device of the internal-combustion engine of this example, The number of rotations of the internal-combustion engine concerned, intake pipe negative pressure, As an intake throttle valve

opening or a fuel supply system. It can also have composition made into the learning control method which

controls the fuel quantity which possesses the sensor which can detect the operating condition in internal-combustion engines, such as injection quantity of ***************, carries out prediction arithmetic of the NO_X flow from the output of the sensor concerned, and is supplied to the reforming catalyst converter of said hydrogen generator.

[0026]And since $NO_{_{\mathbf{Y}}}$ reduction device of the internal-combustion engine of this example makes mixing of

H₂ and exhaust air uniform in the entrance side of said catalyst device, it can possess a mixer or can also consider it as the composition which uses the silencer of an exhaust system effectively. [0027]If it explains in full detail, NO_X reduction device of the internal-combustion engine of this example was invented in order to solve said conventional problem, and shows drawing 1 the basic constitution figure. That is, the 1st point of this example is that this H₂ reduction uses it in the whole drive range of the engine E by the exhaust air low temperature side. The 2nd point is incorporating the H₂ generator 1 into a constitution system in order to enable use by the side of low temperature. The 3rd point is controlling the H₂ generator 1 by the operational status of the engine E, or the amount of NO_X under exhaust air, and enabling it to always expend a polytical exhaust air.

system in order to enable use by the side of low temperature. The 3rd point is controlling the H₂ generator 1 by the operational status of the engine E, or the amount of NO_x under exhaust air, and enabling it to always supply an equivalent grade or superfluous H2 by NO, and a mol during exhaust air. [0028]Since H₂ will react to O₂ and the selectivity of H₂-NO₂ will be lost if exposed to an elevated temperature, the reduction catalyst 2 is arranged near the silencer 3 so that it may not be exposed to not less than 350 **. And this example branches from fuel piping, carries out introductory reforming of the fuel via a flow control valve at the reforming catalyst converter as an H2 generator, and generates H2. H2 is supplied near the entrance of the reduction catalyst 2. In order to make H2 to supply into an equivalent grade by NO_v and the mol under exhaust air, an air content is measured by the suction-air-quantity sensor 5 of the engine E, boil NO_x concentration under exhaust air NO_x sensor 6, after asking for **** and calculating NO_y flow from the output of both the sensors 5 and 6 by the controller 7, It is the composition which controls the air valve for refining by the fuel flow introduced into a reforming catalyst converter in order to generate H₂ corresponding to NO_v flow, and the thing which performs reforming catalyst converter temperature by an exhaust air flow dividing valve, and partial oxidation. [0029]In drawing 5, the delivery late of H_o [as opposed to NO_y in a horizontal axis] and a vertical axis show the reduction rate (purifying rate) of NO_X. If equivalent weight of H(mol) 2 is supplied to NO_X, and NO_X and

the reduction rate (purifying rate) of NO_X. If equivalent weight of H(mol) $_2$ is supplied to NO_X, and NO_X and H $_2$ shall be mixed thoroughly, reduction purifying of all the NO $_X$ will be carried out (theoretical value). However, since complete mixing is not carried out actually, a reduction rate becomes like an experimental value. Although there is a portion to which the purifying rate is good from theory in the experimental value, it is because the steam under exhaust air decomposed on the precious-metals system catalyst and has changed this into H $_2$. Therefore, many H $_2$ reacts to NO $_X$ from supplied H $_2$. [0030]In NO $_X$ reduction device which performs reduction purifying by H $_2$ as other examples, it can be

considered as the function to install the mixer which carries out mixed mixing of H₂ and exhaust air in the entrance side of a reforming catalyst converter. The hydrogen generator and catalyst device which are NO_X purges of others of this example, Since it has a respectively suitable operating temperature range, a reduction catalyst can be installed in the inside of the muffler to which exhaust air expands and temperature falls at 200 ** or less, or its lower stream again in the latter part of the oxidation catalyst which installed the hydrogen generator in the exit of an exhaust manifold in the exhaust system of an internal-combustion engine.

[0031]In NO_X reduction device which supplies H₂ of a hydrogen generator and carries out reduction purifying of the NO_X under engine exhaust gas under O₂ coexistence as other examples, It can have composition which has a means to oxidize HC, such as an oxidation catalyst, a three way component catalyst, and an exhaust air reactor, and CO near an engine exhaust manifold, and uses Pt-zeolitic catalyst for the reforming catalyst converter as a Lean NO_X catalyst. A sound deadening effect can be given to a reforming catalyst converter, and a reforming catalyst converter and an exhaust air muffler can be considered as unification composition.

[0032]And in NO_X purge which performs NO_X reduction by H_2 , it can have composition which installed the soot trapper and the unburnt glow output oxidizing means upstream of the reforming catalyst converter as an object for diesel engines. In this example, a hydrogen fueled engine besides a gasoline engine and a diesel power plant may be sufficient as an internal-combustion engine, and it can be applied effective in these NO_X reduction devices. In the case of this hydrogen fueled engine, a hydrogen generator is not required, and it can be applied by supplying H_2 as fuel in bypass via a controller.

[0033]

[The 1st example] The 1st example that applies the system of this invention to the lean burn engine of the engine displacement 11 is shown in <u>drawing 6</u>. Engine E₁ of the 1st example at the time of the excess air factor lambda= 0.95 at the time of idling - the full load of 1.0 (they are rich side or theoretical air fuel ratio a little than theoretical air fuel ratio) each number of rotations, and rapid acceleration lambda= 0.8-1.0 (rich side), Operating conditions other than this are engine E₁ operated by a thin lambda= 1.2-1.8 side.

Therefore, O₂ under exhaust air changes to about 0 to 10%. Exhaust-system E_y is composition which

installs the oxidation catalyst 9 in the exit of the exhaust manifold 8, oxidizes and purifies incomplete combustion output, such as HC and CO. The reduction catalyst 12 is arranged to the downstream of the muffler 13 as a silencer. In order to equalize mixing with H₂ and exhaust air in the entrance of the reduction catalyst 12, the mixer 10 is formed in it. [0034]The H₂ generator 11 is a water electrolysis H₂ generator using the reforming catalyst 14, as shown in drawing 7 and drawing 8.

[0035]The hydrogen generator 11 forms the coiled inner core in the branched exhaust pipe, the electromagnetism fuel injection valve which injects methanol is provided in one end of the inner core, and the other end is led to the mixer. It is filled up with porous ceramics for near the entrance of the inner core to

Pd. 15 are a suction-air-quantity sensor which measures the air content to engine E_1 among <u>drawing 6</u>, and 16 is a NO_X sensor which measures NO_X concentration under exhaust air. [0036]Since H₂ of the equivalent is needed by NO_X and a mol in the case of the 1st example, are based

evaporate methanol, and the reforming catalyst of the pellet type is got blocked in after that. (When using a monolith-like catalyst, the inner core is changed into linear shape from a coiled form.) The catalyst is using

also on NO_X concentration under exhaust air of engine E_1 , but. In the time of H_2 of 0.3 l/min, and the maximum output maximum horsepower, H_2 of about 1.0 l/min is needed at the time of the vehicle speed of

50 km/h. Although this $\rm H_2$ reforms some fuel and it is supplied, The influence which consumption $\rm H_2$ under each operating condition has on run fuel consumption is 1 to 2% or less, is a grade which can be disregarded if compared with 15 to 20% of the fuel consumption reduction merit using a lean burn engine, and does not spoil the low-fuel-consumption characteristic of a lean burn engine. [0037]The methanol which $\rm H_2$ generating takes is a 0.15 l/min (steam) grade to a 50-km/h run.

[0038]As mentioned above, since the 1st example reforms a little fuel in the $\rm H_2$ generator 11 and performs $\rm H_2\text{-}NO_X$ reduction using the low temperature side characteristic of the reduction catalyst 12, It is a practically significant lean burn $\rm NO_X$ reduction system which can measure reduction of $\rm NO_X$ regardless of the operation excess air factor lambda of engine $\rm E_1$. CO which carries out a byproduction with $\rm H_2$ is a water gas shift

reaction. [0039] [Formula 5]

CO + H2 O -> H2 + CO2

[0040]lt comes out, and changes into H_2 , or Pd film separates into H_2 and CO, and there is also the method of supplying ahead of the reduction catalyst 12 as high grade H_2 . However, CO which carries out a byproduction is little, can be committed in the reduction catalyst 12 as a reducing agent as it is, and does not emit CO. 10041

The 2nd example] The 2nd example is a case of the gas engine used for the object for air conditioning, and power generation. Fuel shows the case of natural gas. Unlike the object for cars, the engine for stationing of such a purpose is operated by the number of certain rotations, and fixed load. Therefore, it is easy to keep the temperature of a reforming catalyst converter constant. Since the composition of the 2nd example is almost the same as that of said 1st example as shown in drawing 9, identical parts attach the same agreement and omit explanation.

[0042]Air and natural gas control the fuel supplied to a hydrogen generator by a regulating valve in order to secure required H_2 which is natural gas, is mixed with air and supplied unlike the 1st example. Control is the same as that of said 1st example almost, and does so the almost same operation effect as said 1st example.

[0043]

[The 3rd example] NO_X reduction device of the engine which combines the device and zeolitic catalyst which reform some fuel and generate H_2 in said each example, and carries out reduction purifying of the NO_X . It has turned out that a big difference is produced for NO_X reduction performance according to the conditions of supply of H_2 , and the contents. As shown in <u>drawing 10</u>, exhaust air of the engine containing NO_X and O_2 is passed for a catalyst, and NO_X purifying rate at the time of supplying H_2 from the upper stream of a reforming catalyst converter is shown in <u>drawing 11</u>. In <u>drawing 11</u>, a horizontal axis shows the supply rate of H_2 to NO_X , and 1.0 is a case where NO_X and H_2 are the equivalents. A vertical axis is the rate that NO_X is purified by reduction, and 1.0 shows that all NO_X will be purified.

[0044]When the catalyst 61 of the pellet type shown in drawing 12 is contained in the reforming catalyst converter 60 shown in drawing 10, a high purifying rate is shown that drawing 14 shows. If the catalyst 62 of the monolith type shown in drawing 13 is used, even if it is the same H2 amount of supply, a purifying rate will fall.

[0045]H $_2$ and exhaust gas do not mix enough the catalyst 61 of the pellet type shown in drawing 12 at the entrance, but even if H₂ has concentration distribution, the crevice between pellets like a maze is enough mixed in the process in which gas is in direct communication and goes, and H2 and exhaust gas are equalized.

[0046]On the other hand, many section "swage block"-like **** have the catalyst 62 of the monolith type shown in drawing 13.

Since the hole of a piece is in the direction of a gas flow independently, if H₂ has distribution at the entrance, it will be hard to mix the gas in the channel which adjoins each other mutually on the way.

According to the actual experiment, it was difficult to make thickness of an exhaust pipe thick substantially from the restrictions on mount, the gas flow rate was quick, H₂ made the high concentration region near the center section, and H₂ has produced the inconvenience hardly supplied in the monolith periphery.

Therefore, the capacity factor of a monolith type of H₂ is low compared with a pellet type.

(0047)On the other hand, when it sees as an engine exhaust gas system, a pellet's rubbing mutually and it being easy to carry out disintegration by vibration and the direct cross-section area of gas of a pellet type are small, pass resistance is large, and causes exhaust-gas-pressure increase, and there is a fault which gets worse in the engine performance itself. Therefore, although it is desirable to use a monolith type for a catalyst, a device is needed for supply of H2 in this case.

[0048]Then, the 3rd example comprises the constitutionally simple device which mixes supply of H₂ homogenously so that NO, purifying rate which was superior to the pellet type using the catalyst of a monolith type may be acquired. That is, the essential structure of the H2 jet nozzle 63 as the mixed device 69 is shown in drawing 14 and drawing 15. The inserted H, jet nozzle 63 is hollow cylinder shape, and it has turned at it in the shape of an L character to the flow direction of exhaust air. It has two or more jet holes 64 radiately.

4-6 pieces are suitable for the radiate jet hole 64 -- one row -- or two or more rows are provided. (Three rows of jet holes are allocated in drawing 14).

[0049]D is required for d not less than 20%, and since resistance of a channel will become large if d is enlarged, the insertion tube outer diameter d of the jet nozzle 63 and the inside diameter D of the exhaust pipe 65 carry out section expansion formation of some exhaust pipes 65, as shown in drawing 16. Even if the distance L from the jet nozzle 63 to the reforming catalyst converter 60 needs more than the twice [at least] of D and enlarges them 10 or more times, there are few improvement effects. The mixed device can show drawing 17 and drawing 18 composition other than ****. that is, the portion which makes H2 stir comprises the H₂ jet nozzle 66 of a byway, and the cylinder like object with base 68 which established two or more jet holes 67 in the wall by the major diameter from this -- about two-fold are constituted tubular. H₂ which blew off is first mixed with the exhaust air which flows into the H2 jet nozzle 66 with the dynamic pressure of exhaust gas pressure, blows off from the container liner of the cylinder like object with base 68 in an outer case, and is further mixed by the exhaust air which flows between inside-and-outside pipes. Thus, since it passes through two steps of mixing processes, about H 2 and exhaust air can mix homogenously thoroughly. [0050]The size (a diameter or a cross-section area) of an inside-and-outside pipe influences mixing greatly, and if a container liner is small, almost all exhaust air flows through an outer case, and cannot use dynamic pressure enough. In drawing 17 and drawing 18, as for D/d (an outer case/container liner), three to about

1,7 are effective, and the two neighborhoods of the diameter ratio of an inside-and-outside pipe are best. [0051]Mixing becomes good, and even if the 3rd example that consists of the above-mentioned composition is a monolith type, it can acquire the same purifying rate as a pellet type. Since the amount of supply H2 can be saved 30 to 60% in the same purifying rate, fuel which $\rm H_2$ generating takes can be lessened and an engine output and the influence on fuel consumption can be reduced. [0052]For example, if the usual operation area representative point estimates in a 1.6-I. lean burn gasoline engine, H₂ flow taken to purify 2000 rpm of engine speed value and torque 40Nm, NO₂ burst size 0.44 l/min at this time, and this NO_x by H₂ reduction is 0.66 l/min. The fuel for H₂ generator becomes fuel vapor of 0.33 I/min generating H₂ of 0.66 I/min (in the case of methanol). [0053]If drawing 17 which is D/d=2, and the device shown in drawing 18 perform mixed promotion, the amount of supply of H₂ can be managed with about 0.44 I/min of NO_x and equivalent weight, and fuel will fall to the steam of steamy 0.22 l/min of 0.22 l/min. That is, it becomes saving of 0.11 l/min.

[0054]

[The 4th example] In said example, hydrogen is generated with a hydrogen generator using a zeolitic catalyst, and if H₂ is supplied to the entrance of a zeolitic catalyst and NO_Y reduction by H₂ is performed, even if high-concentration O2 exists during exhaust air, big NOx purifying rate is acquired. [0055]However, compared with the conventional NO_x catalyst, for example, a three way component catalyst, and Cu-zeolitic catalyst, it is a low-temperature reaction, Compared with the conventional catalyst using the space velocity (ratio of passing gas flow I/hr to the catalyst body product I) 50,000-100,000. SV (for example, 10,000-60,000) small from the relation of reaction velocity must be used. When mounting this system, the reforming catalyst converter of this system consists of inlet gas temperature, the lower stream, for example, near an exhaust air muffler, an exhaust system. However, it is a place in which the large (the

size of a converter is large) reforming catalyst converter of car structure top space velocity is installed in a car, and is hard to apply to all the cars. [0056]Since the 4th example makes installation of a reforming catalyst converter easy, even if it makes a catalyst build in the muffler structure and the muffler for making a Lean NO_x catalyst build in a muffler, and measuring miniaturization, it enables $\mathrm{NO}_{\mathbf{y}}$ purification from temperature conditions.

[0057]That is, since the composition of the 4th example can be managed with one of the two, without

the exhaust air muffler 80 as shown in drawing 20 and drawing 21, it becomes very [in disposition space] advantageous. The reforming catalyst converter 83 which gave the sound deadening effect which built the monolithic catalyst 82 (Pt-zeolite system) in the exhaust air muffler 80 is shown in drawing 20 and drawing 21.

arranging NO_x converter and an exhaust air muffler in series if the Lean NO_x catalyst 82 is made to build in

[0058]While the exhaust air by which mixing mixing was carried out in H2 flows from an arrow direction, it central part, the circulating hole 85 of the mixing plate 84 -- each size -- it differs in a diameter, and since multiple arrays are carried out, passing flow yelocities differ, stirring of gas takes place, and a sound deadening effect is done so by interference. [0059]By the way, as for an exhaust air muffler, it is common to be arranged in engine-exhaust-systems

Osamu's tail end, and since it is cooled on the way, the inlet gas temperature of an exhaust air muffler becomes low. It is 150-200 ** also in the time of the maximum-engine-speed maximum horsepower of an use frequency. [0060]Since sufficient reaction is not expectable unless it is not less than 300-400 **, a catalyst cannot be made to build in in a muffler with the conventional three way component catalyst or the Lean NO_x catalyst of a Cu-zeolite system. In said example, when performing reduction by H₂, it was shown that it can purify at

low temperature, but temperature is about 150-300 **, and if compared with the inlet temperature of an exhaust air muffler, it is in a little high temperature requirement.

component about the activity of NO_x reduction catalyst which supplies H₂ under O₃ coexistence. As a result, Pd and Rh did not have activity, activity of Cu was bad, and Pt found out that high activity was shown. However, Pt needs to be high distribution and carriers which have high specific surface area (more than at least 100-m²/g) for that purpose, such as alumina, silica, and zeolite, are required for it. [0062]this invention persons considered pretreatment which should be performed before the Lean NO_x

[0061]This invention persons examined [various] experimentally what should be selected as a catalyst

catalyst of NO reduction, and H₂ mixing by boiling many things. The result is shown in drawing 19. When $\rm H_2$ is mixed to engine exhaust air and it leads to the Lean $\rm NO_X$ catalyst (Pt system) of $\rm NO_X$ reduction, as

[0063]An afterburner, a reactor, a three way component catalyst, an oxidation catalyst, etc. are established near an engine manifold, When H₂ was supplied and it led to the reforming catalyst converter of NO_Y reduction after oxidizing and carrying out reduction removal of CO and the HC beforehand, as shown in the curve A in drawing 19, active temperature shifted to the low temperature side, and it newly found out that

[0064]In accordance with the inlet temperature of an exhaust air muffler, this temperature was closed. if

shown in the curve B, the peak of activity is near 250 ** among drawing 19.

high activity was shown at 100-150 **.

engine with the highest inlet temperature, and is about 100-150 ** in an operating condition with high normal

flows into the monolithic catalyst 82. Since the circulating hole 85 is not established in the central part which becomes the exhaust flow rate maximum on the mixing plate 84, H2 does not concentrate on the monolith

collides with the mixing plate 84, it passes through the circulating hole 85 of size plurality of this mixing plate 84 and exhaust air and H₂ are enough mixed from the upper stream of the reforming catalyst converter 83, it

muffler 80. After removing HC and CO, the direction which performed NO_X purification by a Lean NO_X catalyst can also improve a purifying rate, and does so the practically outstanding operation effect which does not form soot on a catalyst from the imperfect reaction of HC-O₂. [0065]The sound deadening effect is made more into fitness by installing interference tube Ex1 after the monolithic catalyst 82. <u>Drawing 22</u> does so the same operation effect as <u>drawing 20</u> and <u>drawing 21</u>, and differs in the gestalt of a mixer part with said mixing plate, and the points used as the mixing pipe 86 which is a hollow cylindrical member differ. Since the reforming catalyst converter 83 and the exhaust air muffler 80 can consider the 4th example that consists of the above-mentioned composition as unification composition, it does so the practical effect that it becomes compact and mount nature becomes good, and it does so the outstanding effect which can maintain high NO_x purifying rate in the whole drive range.

possible [for the first time] by building in the reduction catalyst 80 of a Pt-zeolite system in the exhaust air

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TECHNICAL FIELD

[Industrial Application]In what is called the lean burn engine and the diesel power plant, other hydrogen fueled engines, etc. which this invention requires for the nitrogen-oxides reduction device of an internal-combustion engine, and use a lean mixture and aim at the improvement in fuel consumption especially, without it spoils the goodness of the fuel consumption of the engine concerned — the concentration of the oxygen gas $(O_2$ is called below) under exhaust air — it is related with the Lean NO_X catalyst exhaust gas cleaning system which can carry out reduction purifying of the nitrogen oxides $(NO_X$ is called below)

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effectively regardless of how.

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PRIOR ART

[Description of the Prior Art]In a piston engine, as an internal-combustion engine and the Lord, to the reducing method of the nitrogen oxides (NO_X is called below) of exhaust air. The NO_X decreasing method by the use ** Lean NO_X catalyst of the NO_X decreasing method ** super-rarefaction air-fuel ratio by the former and ** three way component catalyst (for example, JP,1-139145,A)

Three ** are considered. However, the weight ratio of the fuel in which the method of ** is supplied to an engine, and air must be about 14.5, i.e., theoretical air fuel ratio. If fuel uses a thin air-fuel ratio from theoretical air fuel ratio, NO_X does not decrease. However, it is known that considering the economical efficiency of fuel consumption specific fuel consumption has few directions which operated the engine by the

thin side from theoretical air fuel ratio as shown in drawing 2, and it is efficient.

[0003]Next, ** tends to reconcile NO $_{\chi}$ reduction and fuel consumption reduction with what is called a lean burn engine. However, if it tries to use the air-fuel ratio which can reduce NO $_{\chi}$ enough, it approaches the misfire limit of combustion, and engine fuel consumption not only worsens, but it will be ruined and drivability will worsen. In order to prevent this, disorder and the increase in the rate of flow are measured with the air flow in a cylinder, the rate of combustion is made quick and there are some which are going to improve a misfire limit so that it may become a thin region more. However, since the flame kernel formation at the time of ignition and the flame propagation in early stages of combustion will be barred on the contrary if air disorder and the increase in the rate of flow are performed too much, there is a limit in expansion of the misfire limit by this method. Although there is also the method of making it into the rich mixture which

adjusted the air-fuel ratio distribution in a cylinder and to which only the neighborhood of an ignition plug was suitable for ignition, since the decreasing rate will decrease as the dashed line also showed generating NO.

if a misfire limit spreads to a thin side more as shown in <u>drawing 3</u>, a big effect is not expectable. [0004]** In order to compensate the fault of the above-mentioned **, it is going to operate using near [slightly near theoretical air fuel ratio] a specific-fuel-consumption minimum score from a misfire limit, and NO_X in which reduction is a little insufficient tends to purify with a zeolite system Lean NO_X catalyst. This method may become a fuel-efficient system. However, there is a problem which should be solved practically

that NO $_{\rm X}$ purifying rate and endurance of catalyst this Lean NO $_{\rm X}$ catalyst will return NO $_{\rm X}$ under a lot of O $_{\rm 2}$ existence during exhaust air, severe [a catalyst] temperature conditions etc. and sufficient under the

present circumstances can be easily incompatible. The method of reducing NO_χ enough all has many practical problems, using the air-fuel ratio which can make engine specific fuel consumption small as much as possible as mentioned above.

[0005]By the way, although it is fundamentally the same that excess O_2 is included during exhaust air also by the lean burn engine or a diesel power plant, O_2 concentration becomes large, so that exhaust air of this engine uses a lean mixture including O_2 during exhaust air. The catalyst which performs NO_X reduction purifying under exhaust air containing such O_2 is called Lean NO_X catalyst, and the catalyst of a preciousmetals system, for example, a zeolite system, is used in many cases. In this Lean NO_X catalyst, the relation between NO_X purifying rate and temperature shows drawing 4. And a not less than 350 ** pyrosphere is mainly a reaction of HC- NO_X . A low temperature region 250-350 ** or less serves as a reduction reaction by H_2 of NO_X , and purification of NO_X is possible for it.

[0006]However, since an exhaust-gas temperature amounts also to a maximum of 800-900 ** since a Lean NO_X catalyst is installed near an engine exhaust manifold, and an air-fuel ratio uses a thin side from theoretical air fuel ratio in exhaust air of a lean burn engine, H₂ hardly exists during exhaust air. Therefore, the characteristic by the side of low temperature was a field which cannot be used conventionally.

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EFFECT OF THE INVENTION

[Function and Effect]NO $_{\rm X}$ reduction device of the internal-combustion engine of this invention which consists of the above-mentioned composition does the following operations so. [0010]Namely, NO $_{\rm X}$ reduction device of the internal-combustion engine of this invention which this invention person etc. invented, The basis of the existence of NO $_{\rm X}$ and O $_{\rm 2}$ during exhaust air according to combustion of supply fuel in the combustion chamber of an internal-combustion engine by having composition as shown in drawing 1, Carry out the catalytic reaction of H $_{\rm 2}$ and the NO $_{\rm X}$, and to the entrance side of nitrogen gas and the catalyst device formed in the exhaust system decomposed into water Methanol or LPG, H $_{\rm 2}$ from the hydrogen generator which leads some hydrocarbon fuel, such as natural gas, to a reforming catalyst converter, and generates H $_{\rm 2}$ is supplied, The operation effect which carries out direct reduction purification

of the NO_{χ} under said exhaust air exactly efficiently by this H $_2$ under the exhaust air low temperature atmosphere in near the silencer of an exhaust system, and reduces this NO_{χ} is done so. For this reason, NO_{χ} reduction device of the internal-combustion engine of this invention, Since an engine operating air-fuel ratio can reduce NO_{χ} according to a catalyst regardless of the concentration of existence of O_2 a thin side and under exhaust air, or O_2 from a rich side, theoretical air fuel ratio, and theoretical air fuel ratio, from theoretical air fuel ratio On engine (car) performance, The profitableness which can choose an optimum value without taking into consideration fuel consumption top NO_{χ} reduction conditions can be given.

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TECHNICAL PROBLEM

conventional various problems, Without spoiling the goodness of the fuel consumption of a lean burn engine or a diesel power plant under coexistence of NO_{x} and O_{y} during exhaust air of a lean burn engine or the diesel power plant always operated by the Oover, (air) side, the concentration of O, under exhaust air -- it is going to provide NO_{χ} reduction device of the exhaust gas cleaning system, i.e., the internal-combustion engine which can control the burst size of $NO_{_{\mathbf{Y}}}$, which carries out reduction purifying of the $NO_{_{\mathbf{Y}}}$ effectively

[Problem(s) to be Solved by the Invention]The purpose of this invention is what solves the above-mentioned

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MEANS

[Means for Solving the Problem] NO_{X} reduction device of an internal-combustion engine of this invention, A basis of existence of NO_{X} and O_{2} during exhaust air by combustion of fuel supplied from a fuel supply system in a combustion chamber of an internal-combustion engine, Form a catalyst device for carrying out catalytic reaction of H_{2} and the NO_{X} within an exhaust system, and purifying NO_{X} , and. Provide a hydrogen generator which generates hydrogen by a reforming catalyst converter for some hydrocarbon fuel, such as methanol or LPG, and natural gas, in an entrance side of this catalyst device, and H_{2} is constituted so that supply is possible, It is the composition of carrying out direct reduction purification of the NO_{X} under said exhaust air by H_{2} from this hydrogen generator under an exhaust air low temperature atmosphere in near the silencer of an exhaust system, and having reduced this NO_{X} .

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EXAMPLE

[Example]A reforming catalyst converter is classified according to the fuel which uses the hydrogen generator in an example for an engine as follows.

[0012]That is, if it is in the engine which uses methanol as fuel, the gas which carried out heating

evaporation of the methanol by exhaust air is led to this catalyst using transition metal catalysts, such as 1Pd, Pt, and Cu/Cr/nickel, and H₂ is generated. About 300 ** is best and catalyst inlet gas temperature is a reaction at this time. [0013]

[Formula 1]

CH₃OH → CO + 2H₂

[0014]It becomes.

[0015]2) Make methanol vapour mix air, according to Cu-nickel-Cr/alumina catalyst, carry out partial oxidation of some methanol, and generate $\rm H_{2^{*}}$ 400 ** - 500 ** are suitable for temperature, it controls the air

flow rate made to mix in methanol, and maintains temperature. The reaction in this case, [0016] [Formula 2]

[0017]It becomes.

[0018]3) Cu-Mn or Cu-Zn is used for a catalyst, and add a steam to methanol, or add air and methanol water, and perform steam reforming. About 250 ** is suitable and temperature is a reaction. [0019]

$$CH_3OH + H_2O \rightarrow 3H_2 + CO_2$$

[0020]It becomes.

[0021]If it is in the engine using hydrocarbon fuel, such as LPG and natural gas, nickel, CO, and Rh are used as a catalyst and it reforms at the temperature of 300-800 **. In the case of this hydrocarbon fuel, the water from a steam, air, or a water tank is added, and refining is carried out to it. (Temperature changes with catalysts.) There is much methane at low temperature and there is much CO at an elevated temperature. As a reaction, 100221

[Formula 4]

```
HC + H_1 O → H_1 + CH_4 + CO_2 300~500°C 
 HC + H_2 O → H_2 + CO + CO_2 800°C 
 HC + A i r → H_3 + CO 800°C 
 HC + 排気 → H_4 + CO 700°C 
 (EGR \& g)
```

[0023]It becomes.

 ${[0024]NO}_\chi$ reduction device of the internal-combustion engine of this example, ${NO}_\chi$ flow is computed from the output of the ${NO}_\chi$ sensor 6 with which the exhaust pipe of said exhaust system is equipped, and the suction-air-quantity sensor 5, It can also have composition which controls the air content and the amount of reforming fuel in the case of performing the engine exhaust gas flow or partial oxidation which determines the always proper amount of ${H}_2$ and heats the reforming catalyst converter as said hydrogen generator. ${[0025]NO}_\chi$ reduction device of the internal-combustion engine of this example, The number of rotations of

the internal-combustion engine concerned, intake pipe negative pressure, As an intake throttle valve opening or a fuel supply system. It can also have composition made into the learning control method which controls the fuel quantity which possesses the sensor which can detect the operating condition in internal-combustion engines, such as injection quantity of ****************, carries out prediction arithmetic of the NO_X flow from the output of the sensor concerned, and is supplied to the reforming catalyst converter of said hydrogen generator.

[0026]And since NO_X reduction device of the internal-combustion engine of this example makes mixing of H_2 and exhaust air uniform in the entrance side of said catalyst device, it can possess a mixer or can also

consider it as the composition which uses the silencer of an exhaust system effectively. [0027]If it explains in full detail, NO_X reduction device of the internal-combustion engine of this example was invented in order to solve said conventional problem, and shows <u>drawing 1</u> the basic constitution figure. That is, the 1st point of this example is that this H₂ reduction uses it in the whole drive range of the engine E by the exhaust air low temperature side. The 2nd point is incorporating the H₂ generator 1 into a constitution system in order to enable use by the side of low temperature. The 3rd point is controlling the H₂ generator 1 by the operational status of the engine E, or the amount of NO_X under exhaust air, and enabling it to always supply an equivalent grade or superfluous H₂ by NO_X and a mol during exhaust air.

[0028]Since $\rm H_2$ will react to $\rm O_2$ and the selectivity of $\rm H_2$ -NO $_{\rm X}$ will be lost if exposed to an elevated temperature, the reduction catalyst 2 is arranged near the silencer 3 so that it may not be exposed to not less than 350 **. And this example branches from fuel piping, carries out introductory reforming of the fuel via a flow control valve at the reforming catalyst converter as an $\rm H_2$ generator, and generates $\rm H_2$. $\rm H_2$ is supplied near the entrance of the reduction catalyst 2. In order to make $\rm H_2$ to supply into an equivalent grade by $\rm NO_{\rm X}$ and the mol under exhaust air, an air content is measured by the suction-air-quantity sensor 5

of the engine E, boil NO_{X} concentration under exhaust air NO_{X} sensor 6, after asking for **** and calculating NO_{X} flow from the output of both the sensors 5 and 6 by the controller 7, It is the composition which controls the air valve for refining by the fuel flow introduced into a reforming catalyst converter in order to generate H_2 corresponding to NO_{X} flow, and the thing which performs reforming catalyst converter temperature by an exhaust air flow dividing valve, and partial oxidation. [0029]In <u>drawing 5</u>, the delivery late of H_2 [as opposed to NO_{X} in a horizontal axis] and a vertical axis show

the reduction rate (purifying rate) of NO_X . If equivalent weight of $H(moi)_2$ is supplied to NO_X , and NO_X and H_2 shall be mixed thoroughly, reduction purifying of all the NO_X will be carried out (theoretical value). However, since complete mixing is not carried out actually, a reduction rate becomes like an experimental value. Although there is a portion to which the purifying rate is good from theory in the experimental value, it is because the steam under exhaust air decomposed on the precious-metals system catalyst and has changed this into H_2 . Therefore, many H_2 reacts to NO_X from supplied H_2 .

[0030]In NO_{X} reduction device which performs reduction purifying by H_{2} as other examples, it can be considered as the function to install the mixer which carries out mixed mixing of H_{2} and exhaust air in the entrance side of a reforming catalyst converter. The hydrogen generator and catalyst device which are NO_{X} purges of others of this example, Since it has a respectively suitable operating temperature range, a reduction catalyst can be installed in the inside of the muffler to which exhaust air expands and temperature falls at 200 ** or less, or its lower stream again in the latter part of the oxidation catalyst which installed the hydrogen generator in the exit of an exhaust manifold in the exhaust system of an internal-combustion

hydrogen generator in the exit of an exhaust manifold in the exhaust system of an internal-combustion engine. [0031]In NO_X reduction device which supplies H₂ of a hydrogen generator and carries out reduction purifying of the NO_X under engine exhaust gas under O₂ coexistence as other examples, It can have composition which has a means to oxidize HC, such as an oxidation catalyst, a three way component catalyst, and an exhaust air reactor, and CO near an engine exhaust manifold, and uses Pt-zeolitic catalyst for the reforming catalyst converter as a Lean NO_X catalyst. A sound deadening effect can be given to a reforming catalyst converter, and a reforming catalyst converter and an exhaust air muffler can be considered as unification composition. [0032]And in NO_X purge which performs NO_X reduction by H₂, it can have composition which installed the soot trapper and the unburnt glow output oxidizing means upstream of the reforming catalyst converter as

soot trapper and the unburnt glow output oxidizing means upstream of the reforming catalyst converter as an object for diesel engines. In this example, a hydrogen fueled engine besides a gasoline engine and a diesel power plant may be sufficient as an internal-combustion engine, and it can be applied effective in these NO_X reduction devices. In the case of this hydrogen fueled engine, a hydrogen generator is not required, and it can be applied by supplying H₂ as fuel in bypass via a controller.

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DESCRIPTION OF DRAWINGS

[Brief Description of the Drawings]
[Drawing 1]The lineblock diagram showing the basic constitution of the example of this invention

[Drawing 2]The diagram showing an air-fuel ratio and the relation of a fuel economy

[Drawing 3]The diagram showing the fuel consumption of a lean burn engine, and the relation of NO_X [Drawing 4]The diagram showing the characteristic of a Lean NO_Y catalyst

[Drawing 5]The diagram showing the relation between H₂ supply rate and NO_X purifying rate

[<u>Drawing 6</u>]The lineblock diagram showing the outline of the 1st example device of this invention [<u>Drawing 7</u>]The sectional view of H₂ generator in the 1st example device

[Drawing 8]The lineblock diagram expanding and showing the important section of H₂ generator of others in

the 1st example device
[<u>Drawing 9</u>]The lineblock diagram showing the outline of the 2nd example device of this invention

[Drawing 10]The lineblock diagram showing the outline of the 3rd example device of this invention

[Drawing 11]The diagram showing the relation of NO_X purifying rate about the 3rd example device

[Drawing 12]The schematic diagram showing pellet type catalyst composition about the 3rd example device

[Drawing 12]The schematic diagram showing pellet type catalyst composition about the 3rd example device [Drawing 13]The schematic diagram showing the catalyst composition of a monolith type about the 3rd example device

[Drawing 14]Drawing of longitudinal section showing the outline of the 3rd example device of this invention [Drawing 15]The cross-sectional view showing the outline of the 3rd example device of this invention [Drawing 16]The schematic diagram showing the outline of the 3rd example device of this invention [Drawing 17]Drawing of longitudinal section showing the example of others of the 3rd example device of this

[Drawing 18] The cross-sectional view showing the example of others of the 3rd example device of this invention

[Drawing 19]The diagram showing NO_X purifying rate situation about the 4th example of this invention [Drawing 20]Drawing of longitudinal section showing the outline of the 4th example device of this invention

[Drawing 20]Drawing of longitudinal section showing the outline of the 4th example device of this invention [Drawing 21]The cross-sectional view showing the outline of the 4th example device of this invention [Drawing 22]Drawing of longitudinal section showing the composition of others of the 4th example device of

[Drawing 22][

invention

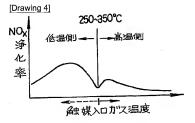
• •		
E, E ₁ engine		
1 and 11 H ₂ generator		
3, 13, and 80 Silencer		
12 and 60 Reduction catalyst		
9 Oxidation catalyst		
5 Suction-air-quantity sensor		
6 NO _X sensor		
7 Control power supply		
10 Mixer		

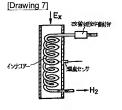
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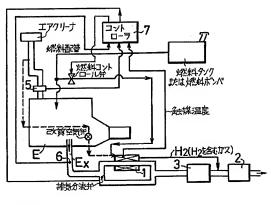
DRAWINGS

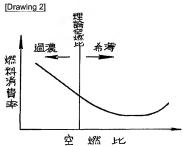


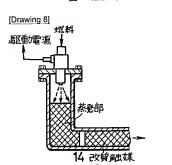


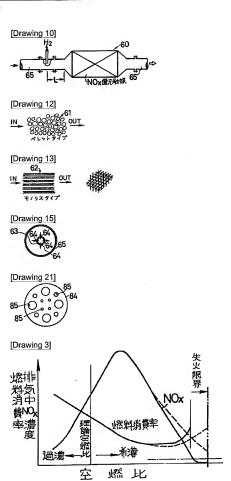


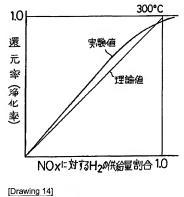
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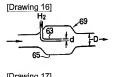


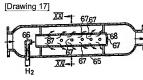




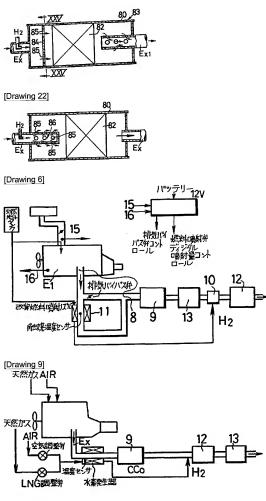








[Drawing 20]



[Drawing 11]

